

Module 4: Lecture 14 to 18

Reynolds Transport Theorem and Navier-Stoke's Equation

Dr. Raj Nandkeolyar

Topics Covered:

1. Reynolds Transport Theorem (RTT).
 - Statement and Derivation of RTT.
 - Integral Form of Conservation of Mass Equation.
2. Conservation of Linear Momentum (Origin of Navier-Stoke's Equation).
 - Derivation of Navier's Equation.
 - Stoke's Hypothesis.
 - Derivation of Navier-Stoke's Equation.

1 Reynolds Transport Theorem (RTT)

This theorem is also known as the **general conservation law** because of the fact that *it provides general form for converting conservation laws from control mass to control volume.*

Consider a control system at time t with some identified mass as shown in the figure. Let the fixed mass occupies the space at time $t + \Delta t$ as shown in the figure.

Let N be the property (*extensive property*) that is being conserved and let n be the value of N per unit mass (*specific property*). Therefore;

$$N_t = (N_I)_t + (N_{II})_t,$$

and $N_{t+\Delta t} = (N_{II})_{t+\Delta t} + (N_{III})_{t+\Delta t}$

Therefore;

$$\begin{aligned} \left. \frac{dN}{dt} \right|_{system} &= \lim_{\Delta t \rightarrow 0} \frac{N_{t+\Delta t} - N_t}{\Delta t} \\ &= \lim_{\Delta t \rightarrow 0} \frac{(N_{II})_{t+\Delta t} - (N_{II})_t}{\Delta t} + \lim_{\Delta t \rightarrow 0} \frac{(N_{III})_{t+\Delta t}}{\Delta t} - \lim_{\Delta t \rightarrow 0} \frac{(N_I)_t}{\Delta t} \end{aligned}$$

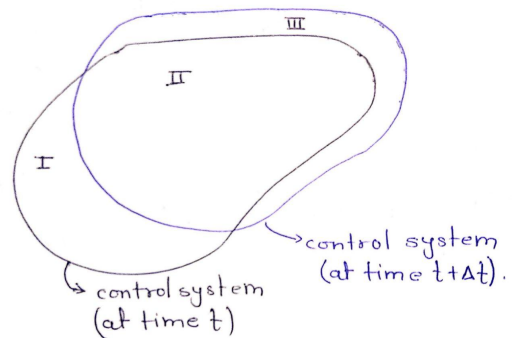


Figure 1: depicting the deformation of control system in Δt time

$$\implies \left. \frac{dN}{dt} \right|_{system} = \left. \frac{\partial N}{\partial t} \right|_{C.V.} + \text{Rate of outflow of } N - \text{Rate of inflow of } N \quad (1)$$

Note that in above equation, we are just writing $\frac{\partial}{\partial t}$ (partial derivative) of N , because it can also be function of different variables. Now;

$$\begin{aligned} \text{mass flow rate from the elementary area } dA &= \rho(\vec{q} \cdot \hat{\eta})dA \\ \text{rate of flow of quantity } N &= n\rho(\vec{q} \cdot \hat{\eta})dA \\ \therefore \text{total rate of flow of } N &= \int_{C.S.} n\rho(\vec{q} \cdot \hat{\eta})dA. \end{aligned}$$

Here the total rate of flow includes both rate of outflow & rate of in flow. Also note that the abbreviated terms $C.V.$ denotes the **Control Volume** whereas $C.S.$ denotes the **Control Surface**. Now, using the value of total rate of flow of N in equation (1), we can write;

$$\left. \frac{dN}{dt} \right|_{system} = \left. \frac{\partial N}{\partial t} \right|_{C.V.} + \int_{C.S.} n\rho(\vec{q} \cdot \hat{\eta})dA$$

$$\begin{aligned} \text{As mass for elementary volume } dV &= \rho dV \\ \implies N &= \int_{C.V.} \rho n dV. \end{aligned}$$

Therefore we get;

$$\left. \frac{dN}{dt} \right|_{system} = \frac{\partial}{\partial t} \int_{C.V.} \rho n dV + \int_{C.S.} n\rho(\vec{q} \cdot \hat{\eta})dA$$

If the control volume is also moving and let \vec{q}_r be the relative velocity of the fluid within the control volume then;

$$\left. \frac{dN}{dt} \right|_{system} = \frac{\partial}{\partial t} \int_{C.V.} \rho n dV + \int_{C.S.} \rho n(\vec{q}_r \cdot \hat{\eta})dA \quad (2)$$

This equation states the **Reynolds transport theorem** or **RTT**.

1.1 Integral Form of Conservation of Mass Equation

By the Reynolds transport theorem *i.e.* equation (2), taking $N = m$ (mass) and therefore $n = 1$ ($\because n = N$ per unit mass) we get;

$$\left. \frac{dm}{dt} \right|_{system} = \frac{\partial}{\partial t} \int_{C.V.} \rho dV + \int_{C.S.} \rho(\vec{q}_r \cdot \hat{\eta})dA$$

As we have considered a control system and therefore we have $\left. \frac{dm}{dt} \right|_{system} = 0$

$$\implies \frac{\partial}{\partial t} \int_{C.V.} \rho dV + \int_{C.S.} \rho(\vec{q}_r \cdot \hat{\eta})dA = 0.$$

Let the control volume be non-deformable (*i.e.* no change *w.r.t.* time) and control volume is also assumed as stationary (*i.e.* $\vec{q}_r = \vec{q}$);

$$\therefore \int_{C.V.} \frac{\partial \rho}{\partial t} dV + \int_{C.S.} \rho \vec{q} \cdot \hat{\eta} dA = 0$$

Now applying divergence theorem *i.e.* $\int_S (\vec{F} \cdot \hat{n}) dA = \int_V (\nabla \cdot \vec{F}) dV$ we get;

$$\begin{aligned} \int_{C.V.} \frac{\partial \rho}{\partial t} dV + \int_{C.V.} \nabla \cdot (\rho \vec{q}) dV &= 0 \\ \implies \int_{C.V.} \left[\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{q}) \right] dV &= 0. \end{aligned} \quad (3)$$

Since the elementary volume dV is arbitrarily chosen, so if integral over dV is zero then integrand is zero. Therefore from equation (3) we get;

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{q}) = 0 \quad (4)$$

The above equation is the conservation of mass equation or the equation of continuity.

2 Conservation of Linear Momentum (Origin of Navier-Stoke's Equation)

Let us assume that control volume is non-deformable and independent of t . We have $N = m\vec{q} = \text{linear momentum}$ and $n = \vec{q}$.

Therefore by the Reynolds transport theorem, we have;

$$\left. \frac{d(m\vec{q})}{dt} \right|_{system} = \frac{\partial}{\partial t} \int_{C.V.} \rho \vec{q} dV + \int_{C.S.} \rho \vec{q} (\vec{q} \cdot \hat{\eta}) dA \quad (5)$$

Further we have;

$$\left. \frac{d(m\vec{q})}{dt} \right|_{system} = m \cdot \left. \frac{d\vec{q}}{dt} \right|_{system} = \sum \vec{F} \Big|_{system}$$

In the limiting case, when $\Delta t \rightarrow 0$, we know that system approaches the control volume;

$$\therefore \sum \vec{F} \Big|_{C.V.} = \frac{\partial}{\partial t} \int_{C.V.} \rho \vec{q} dV + \int_{C.S.} \rho \vec{q} (\vec{q} \cdot \hat{\eta}) dA \quad (6)$$

Writing $x - \text{component}$ of the equation (6);

$$\sum F_{i,C.V.} = \frac{\partial}{\partial t} \int_{C.V.} \rho u_i dV + \int_{C.S.} \rho u_i (\vec{q} \cdot \hat{\eta}) dA \quad (7)$$

We have, resultant force = surface force + body force *i.e.*;

$$\sum F_{i,C.V.} = \int_{C.S.} T_i^\eta dA + \int_{C.V.} \rho b_i dV \quad (8)$$

Further we know that,

$$\begin{aligned} T_i^\eta &= \tau_{i1}\eta_1 + \tau_{i2}\eta_2 + \tau_{i3}\eta_3 \\ \implies T_i^\eta &= (\tau_{i1}\hat{i} + \tau_{i2}\hat{j} + \tau_{i3}\hat{k}) \cdot (\eta_1\hat{i} + \eta_2\hat{j} + \eta_3\hat{k}) \\ \implies T_i^\eta &= \vec{\tau}_i \cdot \hat{\eta} \end{aligned}$$

∴ equation (8) can be written as,
$$\sum F_{i,C.V.} = \int_{C.S.} (\vec{\tau}_i \cdot \hat{n}) dA + \int_{C.V.} \rho b_i dV$$

Using divergence theorem,
$$\sum F_{i,C.V.} = \int_{C.V.} (\nabla \vec{\tau}_i) dV + \int_{C.V.} \rho b_i dV \quad (9)$$

Now using equation (9) in equation (7) we get;

$$\int_{C.V.} (\nabla \vec{\tau}_i) dV + \int_{C.V.} \rho b_i dV = \int_{C.V.} \rho u_i dV + \int_{C.S.} \rho u_i (\vec{q} \cdot \hat{n}) dA$$

$$\Rightarrow \int_{C.V.} (\nabla \vec{\tau}_i) dV + \int_{C.V.} \rho b_i dV = \int_{C.V.} \rho u_i dV + \int_{C.V.} \nabla(\rho u_i \vec{q}) dV \quad [\text{using divergence theorem}]$$

Further solving the above equation;

$$\Rightarrow \int_{C.V.} \left[\frac{\partial}{\partial t}(\rho u_i) + \nabla(\rho u_i \vec{q}) - (\nabla \tau_i) - \rho b_i \right] dV = 0$$

$$\Rightarrow \frac{\partial}{\partial t}(\rho u_i) + \nabla(\rho u_i \vec{q}) - (\nabla \tau_i) - \rho b_i = 0$$

In index notation;

$$\frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) = \frac{\partial}{\partial x_j} \tau_{ij} + \rho b_i \quad (10)$$

We can represent,

$$\tau_{ij} = \tau_{ij}^{hydrostatic} + \tau_{ij}^{deviatoric}. \quad (11)$$

Now, **for further analyzing** $\tau_{ij}^{deviatoric}$: consider;

$$\frac{\partial u_i}{\partial x_j} = \underbrace{\frac{1}{2} \left[\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right]}_{e_{ij}} + \underbrace{\frac{1}{2} \left[\frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right]}_{w_{ij}}.$$

Clearly, e_{ij} is related with the shearing stain rate, $e_{ij} = e_{ji}$ (*i.e.* it's a symmetric tensor). Also, w_{ij} is related with the rotation and $w_{ij} = -w_{ji}$ (*i.e.* it's a skew-symmetric tensor).

Since $\tau_{ij}^{deviatoric}$ is responsible for the shear deformation of the fluid element. Therefore, we have the constitutive relation for the particular fluid;

$$\tau_{ij}^{deviatoric} = f(e_{ij}).$$

Note: For mapping vector to vector, we needed 2^{nd} order tensor & for mapping 2^{nd} order tensor to 2^{nd} order tensor, we need 4^{th} order tensor.

Assuming, the fluid be Newtonian fluid we have;

$$\tau_{ij}^{deviatoric} = c_{ijkl} e_{kl}. \quad (12)$$

Further, let us assume that the fluid is homogeneous (position independent) and isotropic (direction independent).

$$\begin{aligned}
\implies c_{ijkl}A_iB_jC_kD_l &= s \text{ (scalar)} \\
&= \alpha(\vec{A}\cdot\vec{B})(\vec{C}\cdot\vec{D}) + \beta(\vec{A}\cdot\vec{C})(\vec{B}\cdot\vec{D}) + \gamma(\vec{A}\cdot\vec{D})(\vec{B}\cdot\vec{C}) \\
&= \alpha(A_i\cdot B_i)(C_k\cdot D_k) + \beta(A_i\cdot C_i)(B_j\cdot D_j) + \gamma(A_i\cdot D_i)(B_j\cdot C_j) \\
&= \alpha(A_i\delta_{ij}B_j)(C_k\delta_{kl}D_l) + \beta(A_i\delta_{ik}C_k)(B_j\delta_{jl}D_l) + \gamma(A_i\delta_{il}D_l)(B_j\delta_{jk}C_k).
\end{aligned}$$

Comparing;

$$c_{ijkl} = \alpha\delta_{ij}\delta_{kl} + \beta\delta_{ik}\delta_{jl} + \gamma\delta_{il}\delta_{jk}.$$

Here α, β and γ are position independent constants.

We also know that;

$$\begin{aligned}
\tau_{ij}^{deviatoric} &= \tau_{ji}^{deviatoric} \\
\implies c_{ijkl} &= c_{jikl} && \text{[using (12)]} \\
\implies \alpha\delta_{ij}\delta_{kl} + \beta\delta_{ik}\delta_{jl} + \gamma\delta_{il}\delta_{jk} &= \alpha\delta_{ji}\delta_{kl} + \beta\delta_{jk}\delta_{il} + \gamma\delta_{jl}\delta_{ik} \\
\implies \beta &= \gamma.
\end{aligned}$$

Therefore;

$$c_{ijkl} = \alpha\delta_{ij}\delta_{kl} + \beta\delta_{ik}\delta_{jl} + \beta\delta_{il}\delta_{jk}$$

Now,

$$\begin{aligned}
\tau_{ij}^{deviatoric} &= c_{ijkl}\cdot e_{kl} \\
&= \left[\alpha\underbrace{\delta_{kl}}_{k=l} + \beta\underbrace{\delta_{ik}\delta_{jl}}_{k=i, l=j} + \beta\underbrace{\delta_{il}\delta_{jk}}_{l=i, k=j} \right] \cdot e_{kl} \\
&= \alpha\delta_{ij}e_{kk} + \beta e_{ij} + \beta e_{ji}. \\
\therefore \tau_{ij}^{deviatoric} &= \alpha\delta_{ij}e_{kk} + 2\beta e_{ij} && (13)
\end{aligned}$$

Note: Let us understand what is e_{kk} ;

$$\begin{aligned}
e_{ij} &= \frac{1}{2} \left[\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right] \\
\implies e_{kk} &= \frac{\partial u_k}{\partial x_k} \\
&= \frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3} \\
\therefore e_{kk} &= \nabla \cdot \vec{q}.
\end{aligned}$$

Again writing, equation (13) as;

$$\tau_{ij}^{deviatoric} = \lambda\delta_{ij}e_{kk} + \mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right).$$

where, $\mu = \beta =$ coefficient of viscosity & $\lambda = \alpha =$ second coefficient of viscosity.

and

$$\tau_{ij}^{hydrostatic} = -p\delta_{ij}.$$

here, negative sign is for normal component of force/pressure which is opposite to the normal direction.

Therefore, from equation (11), we have a constitutive relationship for a homogeneous, isotropic Newtonian fluid;

$$\tau_{ij} = -p\delta_{ij} + \lambda\delta_{ij}e_{kk} + \mu\left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}\right).$$

Now, assuming that the partial derivatives are continuous;

$$\begin{aligned}\frac{\partial}{\partial x_j}\tau_{ij} &= -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_i}(\lambda e_{kk}) + \frac{\partial}{\partial x_j}\left[\mu\left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}\right)\right] \\ &= -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_i}(\lambda e_{kk}) + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_j}{\partial x_i}\right) \\ &= -\frac{\partial p}{\partial x_i} + \lambda\frac{\partial}{\partial x_i}(e_{kk}) + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + \mu\frac{\partial}{\partial x_i}\left(\frac{\partial u_j}{\partial x_j}\right) \\ \implies \frac{\partial}{\partial x_j}\tau_{ij} &= -\frac{\partial p}{\partial x_i} + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + (\lambda + \mu)\frac{\partial}{\partial x_i}\left(\frac{\partial u_k}{\partial x_k}\right).\end{aligned}\quad (14)$$

Using equation (14) in the equation (10), we get;

$$\frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) = -\frac{\partial p}{\partial x_i} + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + (\lambda + \mu)\frac{\partial}{\partial x_i}\left(\frac{\partial u_k}{\partial x_k}\right) + \rho b_i.\quad (15)$$

This (above) equation is **conservative form of the Navier's equation** for a homogeneous, isotropic Newtonian fluid.

Let us do some more gymnastics (simplifications) for getting the **non-conservative form of the Navier's equation**: simplifying the left side of the equation (15), we get;

$$\begin{aligned}\frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) &= \rho\frac{\partial u_i}{\partial t} + u_i\frac{\partial \rho}{\partial t} + \rho u_j\frac{\partial u_i}{\partial x_j} + u_i\frac{\partial}{\partial x_j}(\rho u_j) \\ &= \rho\frac{\partial u_i}{\partial t} + u_i\left[\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u_j)}{\partial x_j}\right] + \rho u_j\frac{\partial u_i}{\partial x_j} \\ &= \rho\left[\frac{\partial u_i}{\partial t} + u_j\frac{\partial u_i}{\partial x_j}\right] \\ \implies \frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_j}(\rho u_i u_j) &= \rho\frac{Du_i}{Dt}\end{aligned}$$

Therefore, equation (1.16) becomes;

$$\rho\frac{Du_i}{Dt} = -\frac{\partial p}{\partial x_i} + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + (\lambda + \mu)\frac{\partial}{\partial x_i}\left(\frac{\partial u_k}{\partial x_k}\right) + \rho b_i\quad (16)$$

This (above) equation is **non-conservative form of the Navier's equation** for a homogeneous, isotropic Newtonian fluid.

2.1 Stoke's Hypothesis

After doing some more gymnastics with the stress components, we will apply the **Stoke's assumptions (for Stoke's-ian fluids)**;

$$\tau_{ij} = -p\delta_{ij} + \lambda\delta_{ij}e_{kk} + \mu\left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}\right).$$

Taking normal components:

$$\begin{aligned}\tau_{11} &= -p + \lambda e_{kk} + 2\mu\frac{\partial u_1}{\partial x_1} \\ \tau_{22} &= -p + \lambda e_{kk} + 2\mu\frac{\partial u_2}{\partial x_2} \\ \tau_{33} &= -p + \lambda e_{kk} + 2\mu\frac{\partial u_3}{\partial x_3}.\end{aligned}$$

Adding all three stress components, we get;

$$\begin{aligned}\tau_{11} + \tau_{22} + \tau_{33} &= -3p + 3\lambda e_{kk} + 2\mu\left(\frac{\partial u_1}{\partial x_1} + \frac{\partial u_2}{\partial x_2} + \frac{\partial u_3}{\partial x_3}\right) \\ \implies \tau_{11} + \tau_{22} + \tau_{33} &= -3p + 3\lambda e_{kk} + 2\mu e_{kk} \\ \implies \frac{\tau_{11} + \tau_{22} + \tau_{33}}{3} &= -p + \left(\lambda + \frac{2}{3}\mu\right)e_{kk}.\end{aligned}$$

Here, p is the *thermodynamic pressure* and the term $-\frac{\tau_{11} + \tau_{22} + \tau_{33}}{3} = p_m$ is the *mechanical pressure* and therefore, we have;

$$-p_m = -p + \left(\lambda + \frac{2}{3}\mu\right)e_{kk}.$$

From this, we can conclude that: the *mechanical pressure* p_m and the *thermodynamic pressure* p are equal if;

1. $e_{kk} = 0$ (*flow is incompressible*).
2. $\lambda = -\frac{2}{3}\mu$ (**Stoke's hypothesis**).

Note: *Stoke's-ian fluid* is the fluid that satisfies *Stoke's hypothesis* (mentioned above).

Therefore, for a *Stoke's-ian fluid* we have $\lambda = -\frac{2}{3}\mu$ and thus equation (16) becomes;

$$\rho\frac{Du_i}{Dt} = -\frac{\partial p}{\partial x_i} + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + \frac{\mu}{3}\frac{\partial}{\partial x_i}\left(\frac{\partial u_k}{\partial x_k}\right) + \rho b_i \quad (17)$$

If flow is incompressible *i.e.* $e_{kk} = 0$, and therefore;

$$\rho\frac{Du_i}{Dt} = -\frac{\partial p}{\partial x_i} + \mu\frac{\partial}{\partial x_j}\left(\frac{\partial u_i}{\partial x_j}\right) + \rho b_i. \quad (18)$$

This (above) equation is the ***simplest form of the Navier-Stoke's equation***.

Writing the $x - \text{component}$ (similarly we can write other components) of this equation;

$$\rho \frac{Du_1}{Dt} = -\frac{\partial p}{\partial x_1} + \mu \sum_{j=1}^3 \frac{\partial}{\partial x_j} \left(\frac{\partial u_1}{\partial x_j} \right) + \rho b_1$$

Or

$$\rho \frac{Du_1}{Dt} = -\frac{\partial p}{\partial x_1} + \mu \left[\frac{\partial^2 u_1}{\partial x_1^2} + \frac{\partial^2 u_1}{\partial x_2^2} + \frac{\partial^2 u_1}{\partial x_3^2} \right] + \rho b_1.$$

Vector form of the Navier-Stoke's equation can be written as;

$$\rho \frac{D\vec{q}}{Dt} = -\nabla p + \mu \nabla^2 \vec{q} + \rho \vec{b}. \quad (19)$$

Thus we are done with the Navier-Stoke's equation for a viscous, incompressible, homogeneous, isotropic Newtonian fluid flow. Further for our satisfaction, we can check the *dimensional homogeneity* of this equation.

